

IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Original): A process for preparing trichlorosilan (HSiCl_3) by catalytic hydrodehalogenation of silicon tetrachloride (SiCl_4) in the presence of hydrogen, in which at least one metal or metal salt selected from among the elements of main group 2 of the Periodic Table of the Elements is used as catalyst at a temperature in the range from 300 to 1000°C .

Claim 2 (Original): The process as claimed in claim 1,
wherein
calcium, strontium, barium, calcium chloride, strontium chloride, barium chloride or a mixture of at least two of the abovementioned components is used as catalyst.

Claim 3 (Currently Amended): The process as claimed in claim 1 ~~[[or 2]]~~,
wherein
a supported catalyst is used.

Claim 4 (Currently Amended): The process as claimed in ~~any of claims 1 to 3~~ claim
1,
wherein
a catalyst which has been applied to a support selected from the group consisting of low-aluminum zeolites, leached glass, fused silica, activated carbon, porous siliceous supports or SiO_2 supports is used.

Claim 5 (Currently Amended): The process as claimed in ~~any of claims 1 to 4~~ claim 1,
wherein
the supported catalyst used has a catalyst content, calculated as element, of from 0.1 to 10% by weight.

Claim 6 (Currently Amended): The process as claimed in ~~any of claims 1 to 5~~ claim 1,
wherein
an SiCl_4/H_2 mixture having a molar ratio of from 1:0.9 to 1:20 is brought into contact with the catalyst.

Claim 7 (Currently Amended): The process as claimed in ~~any of claims 1 to 6~~ claim 1,
wherein
the reaction is carried out in a fixed-bed reactor, in a fluidized-bed reactor or in a moving-bed reactor.

Claim 8 (Currently Amended): The process as claimed in ~~any of claims 1 to 7~~ claim 1,
wherein
the catalytic reaction is carried out at a temperature in the range from 600 to 950°C and a pressure of from 0.1 to 100 bar abs.

Claim 9 (Currently Amended): The process as claimed in ~~any of claims 1 to 8~~ claim
1,
wherein
the reaction is carried out at a space velocity of from 2000 to 30000 h⁻¹ and the gas
stream has a linear velocity of from 0.01 to 10 m/s in the reactor.

Claim 10 (Currently Amended): The process as claimed in ~~any of claims 1 to 9~~ claim
1,
wherein
HSiCl₃ is isolated from the product mixture or the product mixture is used further
directly.